For sheet steel, take $\varepsilon \approx 0.00015$ ft, hence $\varepsilon/D_h \approx 0.000346$. Now relate everything to the input power:

Power = 1 hp = 550
$$\frac{\text{ft} \cdot \text{lbf}}{\text{s}} = \rho \text{gQh}_{\text{f}} = (0.00234)(32.2)\text{Q}[54.4\text{fQ}^2],$$

or: $\text{fQ}^3 \approx 134$ with Q in ft³/s
Guess $\text{f} \approx 0.02, \quad \text{Q} = (134/0.02)^{1/3} \approx 18.9 \quad \frac{\text{ft}^3}{\text{s}}, \quad \text{Re} = \frac{\rho(\text{Q}/\text{A})\text{D}_{\text{h}}}{\mu} \approx 209000$

Iterate: fbetter ≈ 0.0179 , Qbetter ≈ 19.6 ft³/s, Rebetter ≈ 216500 . The process converges to

$$f \approx 0.01784$$
, $V \approx 80.4$ ft/s, $Q \approx 19.6$ ft³/s. Ans.

6.91 Heat exchangers often consist of many triangular passages. Typical is Fig. P6.91, with L = 60 cm and an isoscelestriangle cross section of side length a = 2 cm and included angle $\beta = 80^{\circ}$. If the average velocity is V = 2 m/s and the fluid is SAE 10 oil at 20°C, estimate the pressure drop.



Solution: For SAE 10 oil, take $\rho = 870 \text{ kg/m}^3$ and $\mu = 0.104 \text{ kg/m} \cdot \text{s}$. The Reynolds number based on side length *a* is Re = $\rho \text{Va}/\mu \approx 335$, so the flow is *laminar*. The bottom side of the triangle is 2(2 cm)sin40° ≈ 2.57 cm. Calculate hydraulic diameter:

$$A = \frac{1}{2} (2.57)(2\cos 40^{\circ}) \approx 1.97 \text{ cm}^2; \quad P = 6.57 \text{ cm}; \quad D_h = \frac{4A}{P} \approx 1.20 \text{ cm}$$
$$Re_{D_h} = \frac{\rho V D_h}{\mu} = \frac{870(2.0)(0.0120)}{0.104} \approx 201; \quad \text{from Table 6.4, } \theta = 40^{\circ}, \quad \text{fRe} \approx 52.9$$
$$Then \quad f = \frac{52.9}{201} \approx 0.263, \quad \Delta p = f \frac{L}{D_h} \frac{\rho}{2} V^2 = (0.263) \left(\frac{0.6}{0.012}\right) \left(\frac{870}{2}\right) (2)^2$$
$$\approx 23000 \text{ Pa} \quad Ans.$$