

**12-46** Water flows over a large plate. The rate of heat transfer per unit width of the plate is to be determined.

**Assumptions** 1 Steady operating conditions exist. 2 The critical Reynolds number is  $Re_{cr} = 5 \times 10^5$ . 3 Radiation effects are negligible.

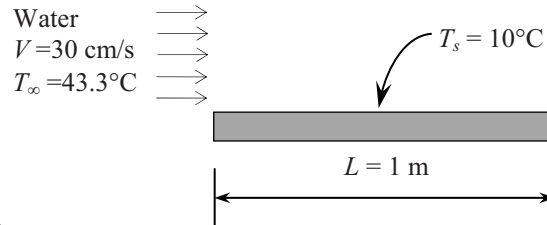
**Properties** The properties of water at the film temperature of  $(T_s + T_\infty)/2 = (10 + 43.3)/2 = 27^\circ\text{C}$  are (Table A-15)

$$\rho = 996.6 \text{ kg/m}^3$$

$$k = 0.610 \text{ W/m}\cdot^\circ\text{C}$$

$$\mu = 0.854 \times 10^{-3} \text{ kg/m}\cdot\text{s}$$

$$Pr = 5.85$$



**Analysis** (a) The Reynolds number is

$$Re_L = \frac{VL\rho}{\mu} = \frac{(0.3 \text{ m/s})(1.0 \text{ m})(996.6 \text{ kg/m}^3)}{0.854 \times 10^{-3} \text{ m}^2/\text{s}} = 3.501 \times 10^5$$

which is smaller than the critical Reynolds number. Thus we have laminar flow for the entire plate. The Nusselt number and the heat transfer coefficient are

$$Nu = 0.664 Re_L^{1/2} Pr^{1/3} = 0.664(3.501 \times 10^5)^{1/2} (5.85)^{1/3} = 707.9$$

$$h = \frac{k}{L} Nu = \frac{0.610 \text{ W/m}\cdot^\circ\text{C}}{1.0 \text{ m}} (707.9) = 431.8 \text{ W/m}^2 \cdot ^\circ\text{C}$$

Then the rate of heat transfer per unit width of the plate is determined to be

$$\dot{Q} = hA_s(T_s - T_\infty) = (431.8 \text{ W/m}^2 \cdot ^\circ\text{C})(1 \text{ m})(1 \text{ m})(43.3 - 10)^\circ\text{C} = \mathbf{14,400 \text{ W}}$$