

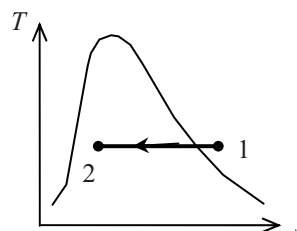
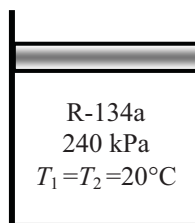
8-52 R-134a undergoes an isothermal process in a closed system. The work and heat transfer are to be determined.

Assumptions 1 The system is stationary and thus the kinetic and potential energy changes are zero. **2** There are no work interactions involved other than the boundary work. **3** The thermal energy stored in the cylinder itself is negligible. **4** The compression or expansion process is quasi-equilibrium.

Analysis The energy balance for this system can be expressed as

$$\underbrace{E_{\text{in}} - E_{\text{out}}}_{\text{Net energy transfer by heat, work, and mass}} = \underbrace{\Delta E_{\text{system}}}_{\text{Change in internal, kinetic, potential, etc. energies}}$$

$$W_{\text{in}} - Q_{\text{out}} = \Delta U = m(u_2 - u_1)$$



The initial state properties are

$$\left. \begin{array}{l} P_1 = 240 \text{ kPa} \\ T_1 = 20^\circ\text{C} \end{array} \right\} \begin{array}{l} u_1 = 246.74 \text{ kJ/kg} \\ s_1 = 1.0134 \text{ kJ/kg} \cdot \text{K} \end{array} \quad (\text{Table A-13})$$

For this isothermal process, the final state properties are (Table A-11)

$$\left. \begin{array}{l} T_2 = T_1 = 20^\circ\text{C} \\ x_2 = 0.20 \end{array} \right\} \begin{array}{l} u_2 = u_f + x_2 u_{fg} = 78.86 + (0.20)(162.16) = 111.29 \text{ kJ/kg} \\ s_2 = s_f + x_2 s_{fg} = 0.30063 + (0.20)(0.62172) = 0.42497 \text{ kJ/kg} \cdot \text{K} \end{array}$$

The heat transfer is determined from

$$q_{\text{in}} = T_0 (s_2 - s_1) = (293 \text{ K})(0.42497 - 1.0134) \text{ kJ/kg} \cdot \text{K} = -172.4 \text{ kJ/kg}$$

The negative sign shows that the heat is actually transferred from the system. That is,

$$q_{\text{out}} = \mathbf{172.4 \text{ kJ/kg}}$$

The work required is determined from the energy balance to be

$$w_{\text{in}} = q_{\text{out}} + (u_2 - u_1) = 172.4 \text{ kJ/kg} + (111.29 - 246.74) \text{ kJ/kg} = \mathbf{36.95 \text{ kJ/kg}}$$

8-53 The total heat transfer for the process 1-3 shown in the figure is to be determined.

Analysis For a reversible process, the area under the process line in T-s diagram is equal to the heat transfer during that process. Then,

$$\begin{aligned} Q_{1-3} &= Q_{1-2} + Q_{2-3} \\ &= \int_1^2 T dS + \int_2^3 T dS \\ &= \frac{T_1 + T_2}{2} (S_2 - S_1) + T_2 (S_3 - S_2) \\ &= \frac{(360 + 273) + (55 + 273) \text{ K}}{2} (3 - 1) \text{ kJ/K} + (360 + 273 \text{ K})(2 - 3) \text{ kJ/K} \\ &= \mathbf{328 \text{ kJ}} \end{aligned}$$

