10-97E A geothermal power plant operating on the simple Rankine cycle using an organic fluid as the working fluid is considered. The exit temperature of the geothermal water from the vaporizer, the rate of heat rejection from the working fluid in the condenser, the mass flow rate of geothermal water at the preheater, and the thermal efficiency of the Level I cycle of this plant are to be determined.

Assumptions 1 Steady operating conditions exist. 2 Kinetic and potential energy changes are negligible.

Analysis (*a*) The exit temperature of geothermal water from the vaporizer is determined from the steady-flow energy balance on the geothermal water (brine),

$$\dot{Q}_{\text{brine}} = \dot{m}_{\text{brine}} c_p (T_2 - T_1)$$

- 22,790,000 Btu/h = (384,286 lbm/h)(1.03 Btu/lbm · °F)(T_2 - 325°F)
 $T_2 = 267.4$ °F

(b) The rate of heat rejection from the working fluid to the air in the condenser is determined from the steady-flow energy balance on air,

$$\dot{Q}_{air} = \dot{m}_{air} c_p (T_9 - T_8)$$

= (4,195,100 lbm/h)(0.24 Btu/lbm·°F)(84.5-55°F)
= **29.7 MBtu/h**

(c) The mass flow rate of geothermal water at the preheater is determined from the steady-flow energy balance on the geothermal water,

$$\dot{Q}_{\text{geo}} = \dot{m}_{\text{geo}} c_p (T_{\text{out}} - T_{\text{in}})$$

-11,140,000 Btu/h = $\dot{m}_{\text{geo}} (1.03 \text{ Btu/lbm} \cdot {}^\circ\text{F})(154.0 - 211.8 {}^\circ\text{F})$
 $\dot{m}_{\text{geo}} = \mathbf{187,120 \ lbm/h}$

(d) The rate of heat input is

$$\dot{Q}_{in} = \dot{Q}_{vaporizer} + \dot{Q}_{reheater} = 22,790,000 + 11,140,000$$

= 33,930,000 Btu / h

and

$$\dot{W}_{\text{net}} = 1271 - 200 = 1071 \text{ kW}$$

Then,

$$\eta_{\rm th} = \frac{\dot{W}_{\rm net}}{\dot{Q}_{\rm in}} = \frac{1071 \text{ kW}}{33,930,000 \text{ Btu/h}} \left(\frac{3412.14 \text{ Btu}}{1 \text{ kWh}}\right) = 10.8\%$$