**11-14** An ideal vapor-compression refrigeration cycle with refrigerant-134a as the working fluid is considered. The rate of heat removal from the refrigerated space, the power input to the compressor, the rate of heat rejection to the environment, and the COP are to be determined.

Assumptions 1 Steady operating conditions exist. 2 Kinetic and potential energy changes are negligible.

*Analysis* (a) In an ideal vapor-compression refrigeration cycle, the compression process is isentropic, the refrigerant enters the compressor as a saturated vapor at the evaporator pressure, and leaves the condenser as saturated liquid at the condenser pressure. From the refrigerant tables (Tables A-12 and A-13),

$$\begin{array}{l} P_1 = 120 \text{ kPa} \\ \text{sat. vapor} \end{array} \} h_1 = h_{g @ 120 \text{ kPa}} = 236.97 \text{ kJ/kg} \\ sat. \text{vapor} \end{array} \} s_1 = s_{g @ 120 \text{ kPa}} = 0.94779 \text{ kJ/kg} \cdot \text{K} \\ P_2 = 0.7 \text{ MPa} \\ s_2 = s_1 \end{array} \} h_2 = 273.50 \text{ kJ/kg} \left( T_2 = 34.95^{\circ}\text{C} \right) \\ P_3 = 0.7 \text{ MPa} \\ \text{sat. liquid} \end{cases} h_3 = h_{f @ 0.7 \text{ MPa}} = 88.82 \text{ kJ/kg} \\ h_4 \cong h_3 = 88.82 \text{ kJ/kg} \left( \text{throttling} \right) \end{array}$$

Then the rate of heat removal from the refrigerated space and the power input to the compressor are determined from

$$\dot{Q}_L = \dot{m}(h_1 - h_4) = (0.05 \text{ kg/s})(236.97 - 88.82) \text{ kJ/kg} = 7.41 \text{ kW}$$

and

$$\dot{W}_{\rm in} = \dot{m}(h_2 - h_1) = (0.05 \text{ kg/s})(273.50 - 236.97) \text{ kJ/kg} = 1.83 \text{ kW}$$

(b) The rate of heat rejection to the environment is determined from

$$\dot{Q}_H = \dot{Q}_L + \dot{W}_{in} = 7.41 + 1.83 = 9.23 \text{ kW}$$

(c) The COP of the refrigerator is determined from its definition,

$$COP_R = \frac{\dot{Q}_L}{\dot{W}_{in}} = \frac{7.41 \text{ kW}}{1.83 \text{ kW}} = 4.06$$

