**8-36** An insulated cylinder is initially filled with saturated liquid water at a specified pressure. The water is heated electrically at constant pressure. The minimum work by which this process can be accomplished and the exergy destroyed are to be determined.

*Assumptions* **1** The kinetic and potential energy changes are negligible. **2** The cylinder is well-insulated and thus heat transfer is negligible. **3** The thermal energy stored in the cylinder itself is negligible. **4** The compression or expansion process is quasi-equilibrium.

Analysis (a) From the steam tables (Tables A-4 through A-6),

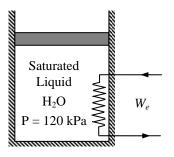
$$u_{1} = u_{f @ 120 \text{ kPa}} = 439.27 \text{ kJ / kg}$$

$$P_{1} = 120 \text{ kPa} \quad v_{1} = v_{f @ 120 \text{ kPa}} = 0.001047 \text{ m}^{3}/\text{kg}$$
sat. liquid
$$\int h_{1} = h_{f @ 120 \text{ kPa}} = 439.36 \text{ kJ/kg}$$

$$s_{1} = s_{f @ 120 \text{ kPa}} = 1.3609 \text{ kJ/kg} \cdot \text{K}$$

The mass of the steam is

$$m = \frac{\nu}{\nu_1} = \frac{0.008 \text{ m}^3}{0.001047 \text{ m}^3 / \text{kg}} = 7.639 \text{ kg}$$



We take the contents of the cylinder as the system. This is a closed system since no mass enters or leaves. The energy balance for this stationary closed system can be expressed as

$$\underbrace{E_{\text{in}} - E_{\text{out}}}_{\text{Net energy transfer}} = \underbrace{\Delta E_{\text{system}}}_{\text{Change in internal, kinetic, potential, etc. energies}}$$
$$W_{\text{e,in}} - W_{\text{b,out}} = \Delta U$$
$$W_{\text{e,in}} = m(h_2 - h_1)$$

since  $\Delta U + W_b = \Delta H$  during a constant pressure quasi-equilibrium process. Solving for  $h_2$ ,

$$h_2 = h_1 + \frac{W_{e,in}}{m} = 439.36 + \frac{1400 \text{ kJ}}{7.639 \text{ kg}} = 622.63 \text{ kJ/kg}$$

Thus,

$$P_{2} = 120 \text{ kPa}$$

$$h_{2} = 622.63 \text{ kJ/kg}$$

$$\begin{cases}
x_{2} = \frac{h_{2} - h_{f}}{h_{fg}} = \frac{622.63 - 439.36}{2243.7} = 0.08168 \\
s_{2} = s_{f} + x_{2}s_{fg} = 1.3609 + 0.08168 \times 5.93687 = 1.8459 \text{ kJ/kg} \cdot \text{K} \\
u_{2} = u_{f} + x_{2}u_{fg} = 439.24 + 0.08168 \times 2072.4 = 608.52 \text{ kJ/kg} \\
v_{2} = v_{f} + x_{2}v_{fg} = 0.001047 + 0.08168 \times (1.4285 - 0.001047) = 0.1176 \text{ m}^{3}/\text{kg}
\end{cases}$$

The reversible work input, which represents the minimum work input  $W_{rev,in}$  in this case can be determined from the exergy balance by setting the exergy destruction equal to zero,

$$\underbrace{X_{\text{in}} - X_{\text{out}}}_{\text{Net exergy trasfer}} - \underbrace{X_{\text{destroyed}}}_{\text{Exergy}} - \underbrace{\Delta X_{\text{system}}}_{\text{change}} \rightarrow W_{\text{rev,in}} = X_2 - X_1$$

Substituting the closed system exergy relation, the reversible work input during this process is determined to be  $W_{\text{rev,in}} = -m[(u_1 - u_2) - T_0(s_1 - s_2) + P_0(\boldsymbol{v}_1 - \boldsymbol{v}_2)]$ 

$$= -(7.639 \text{ kg})\{(439.27 - 608.52) \text{ kJ/kg} - (298 \text{ K})(1.3609 - 1.8459) \text{ kJ/kg} \cdot \text{K} + (100 \text{ kPa})(0.001047 - 0.1176)\text{m}^3 / \text{kg}[1 \text{ kJ/1 kPa} \cdot \text{m}^3]\}$$

(b) The exergy destruction (or irreversibility) associated with this process can be determined from its definition  $X_{\text{destroyed}} = T_0 S_{\text{gen}}$  where the entropy generation is determined from an entropy balance on the cylinder, which is an insulated closed system,

$$\underbrace{S_{\text{in}} - S_{\text{out}}}_{\text{by heat and mass}} + \underbrace{S_{\text{gen}}}_{\text{Entropy}} = \underbrace{\Delta S_{\text{system}}}_{\text{in entropy}}$$

$$S_{\text{gen}} = \Delta S_{\text{system}} = m(s_2 - s_1)$$

Substituting,

$$X_{\text{destroved}} = T_0 S_{\text{gen}} = mT_0 (s_2 - s_1) = (298 \text{ K})(7.639 \text{ kg})(1.8459 - 1.3609) \text{kJ/kg} \cdot \text{K} = 1104 \text{ kJ}$$

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