12-41 Wind is blowing parallel to the wall of a house. The rate of heat loss from that wall is to be determined for two cases.

Assumptions 1 Steady operating conditions exist. 2 The critical Reynolds number is $Re_{cr} = 5 \times 10^5$. 3 Radiation effects are negligible. 4 Air is an ideal gas with constant properties.

Properties The properties of air at 1 atm and the

film temperature of $(T_s + T_{\infty})/2 = (12+5)/2 =$ 8.5°C are (Table A-22) $k = 0.02428 \text{ W/m} \cdot ^{\circ}\text{C}$ $v = 1.413 \times 10^{-5} \text{ m}^2/\text{s}$ Pr = 0.7340Analysis Air flows parallel to the 10 m side: The Reynolds number in this case is $\text{Re}_{T_s} = \frac{VL}{L} = \frac{[(55 \times 1000 / 3600) \text{ m/s}](10 \text{ m})}{[(10 \text{ m})](10 \text{ m})} = 1.081 \times 10^7$

$$\operatorname{Re}_{L} = \frac{VL}{v} = \frac{\left[(55 \times 1000 / 3600) \operatorname{m/s}\right](10 \operatorname{m})}{1.413 \times 10^{-5} \operatorname{m}^{2}/\mathrm{s}} = 1.081 \times 10^{-5} \operatorname{m}^{2}/\mathrm{s}$$

which is greater than the critical Reynolds number. Thus we have combined laminar and turbulent flow. Using the proper relation for Nusselt number, heat transfer coefficient and then heat transfer rate are determined to be

$$Nu = \frac{hL}{k} = (0.037 \text{ Re}_{L}^{0.8} - 871) \text{ Pr}^{1/3} = [0.037(1.081 \times 10^{7})^{0.8} - 871](0.7340)^{1/3} = 1.336 \times 10^{4}$$
$$h = \frac{k}{L} Nu = \frac{0.02428 \text{ W/m.°C}}{10 \text{ m}} (1.336 \times 10^{4}) = 32.43 \text{ W/m}^{2}.°\text{C}$$
$$A_{s} = wL = (4 \text{ m})(10 \text{ m}) = 40 \text{ m}^{2}$$
$$\dot{Q} = hA_{s} (T_{\infty} - T_{s}) = (32.43 \text{ W/m}^{2}.°\text{C})(40 \text{ m}^{2})(12 - 5)°\text{C} = 9080 \text{ W} = 9.08 \text{ kW}$$

If the wind velocity is doubled:

$$\operatorname{Re}_{L} = \frac{VL}{V} = \frac{\left[(110 \times 1000 / 3600) \text{m/s}\right](10 \text{ m})}{1.413 \times 10^{-5} \text{ m}^{2}/\text{s}} = 2.162 \times 10^{7}$$

which is greater than the critical Reynolds number. Thus we have combined laminar and turbulent flow. Using the proper relation for Nusselt number, the average heat transfer coefficient and the heat transfer rate are determined to be

$$Nu = \frac{hL}{k} = (0.037 \text{ Re}_{L}^{0.8} - 871) \text{ Pr}^{1/3} = [0.037(2.162 \times 10^{7})^{0.8} - 871](0.7340)^{1/3} = 2.384 \times 10^{4}$$
$$h = \frac{k}{L} Nu = \frac{0.02428 \text{ W/m.}^{\circ}\text{C}}{10 \text{ m}} (2.384 \times 10^{4}) = 57.88 \text{ W/m}^{2}.^{\circ}\text{C}$$
$$\dot{Q} = hA_{s} (T_{\infty} - T_{s}) = (57.88 \text{ W/m}^{2}.^{\circ}\text{C})(40 \text{ m}^{2})(12 - 5)^{\circ}\text{C} = 16,210 \text{ W} = 16.21 \text{ kW}$$