**14-29** A printed circuit board (PCB) is placed in a room. The average temperature of the hot surface of the board is to be determined for different orientations.

*Assumptions* 1 Steady operating conditions exist. 2 Air is an ideal gas with constant properties. 3 The local atmospheric pressure is 1 atm. 3 The heat loss from the back surface of the board is negligible.

**Properties** The properties of air at 1 atm and the anticipated film temperature of  $(T_s+T_\infty)/2 = (45+20)/2 = 32.5$ °C are (Table A-22)

$$k = 0.02607 \text{ W/m.°C}$$

$$v = 1.631 \times 10^{-5} \text{ m}^2/\text{s}$$

$$Pr = 0.7275$$

$$\beta = \frac{1}{T_f} = \frac{1}{(32.5 + 273)\text{K}} = 0.003273 \text{ K}^{-1}$$



*Analysis* The solution of this problem requires a trial-and-error approach since the determination of the Rayleigh number and thus the Nusselt number depends on the surface temperature which is unknown

(a) Vertical PCB. We start the solution process by "guessing" the surface temperature to be 45°C for the evaluation of the properties and *h*. We will check the accuracy of this guess later and repeat the calculations if necessary. The characteristic length in this case is the height of the PCB,  $L_c = L = 0.2$  m. Then,

$$Ra = \frac{g\beta(T_s - T_{\infty})L^3}{v^2} \operatorname{Pr} = \frac{(9.81 \text{ m/s}^2)(0.003273 \text{ K}^{-1})(45 - 20 \text{ K})(0.2 \text{ m})^3}{(1.631 \times 10^{-5} \text{ m}^2/\text{s})^2} (0.7275) = 1.756 \times 10^7$$

$$\operatorname{Nu} = \left\{ 0.825 + \frac{0.387 \text{Ra}^{1/6}}{\left[1 + \left(\frac{0.492}{\text{Pr}}\right)^{9/16}\right]^{8/27}}\right\}^2 = \left\{ 0.825 + \frac{0.387(1.756 \times 10^7)^{1/6}}{\left[1 + \left(\frac{0.492}{0.7275}\right)^{9/16}\right]^{8/27}}\right\}^2 = 36.78$$

$$h = \frac{k}{L} Nu = \frac{0.02607 \text{ W/m.}^{\circ}\text{C}}{0.2 \text{ m}} (36.78) = 4.794 \text{ W/m}^2.^{\circ}\text{C}$$

$$A_s = (0.15 \text{ m})(0.2 \text{ m}) = 0.03 \text{ m}^2$$

Heat loss by both natural convection and radiation heat can be expressed as

$$\dot{Q} = hA_s (T_s - T_{\infty}) + \varepsilon A_s \sigma (T_s^4 - T_{surr}^4)$$

$$8 W = (4.794 W/m^2.^{\circ}C)(0.03 m^2)(T_s - 20)^{\circ}C + (0.8)(0.03 m^2)(5.67 \times 10^{-8}) [(T_s + 273)^4 - (20 + 273 K)^4]$$
solution is

Its solution is

$$T_s = 46.6^{\circ} C$$

which is sufficiently close to the assumed value of  $45^{\circ}$ C for the evaluation of the properties and *h*. (*b*) **Horizontal, hot surface facing up** Again we assume the surface temperature to be  $45^{\circ}$ C and use the properties evaluated above. The characteristic length in this case is

$$L_c = \frac{A_s}{p} = \frac{(0.20 \text{ m})(0.15 \text{ m})}{2(0.2 \text{ m} + 0.15 \text{ m})} = 0.0429 \text{ m}.$$

Then

$$Ra = \frac{g\beta(T_s - T_{\infty})L_c^3}{v^2} \Pr = \frac{(9.81 \text{ m/s}^2)(0.003273 \text{ K}^{-1})(45 - 20 \text{ K})(0.0429 \text{ m})^3}{(1.631 \times 10^{-5} \text{ m}^2/\text{s})^2} (0.7275) = 1.728 \times 10^5$$

$$Nu = 0.54Ra^{1/4} = 0.54(1.728 \times 10^5)^{1/4} = 11.01$$

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$$h = \frac{k}{L_c} Nu = \frac{0.02607 \text{ W/m.}^{\circ}\text{C}}{0.0429 \text{ m}} (11.01) = 6.696 \text{ W/m}^2.^{\circ}\text{C}$$

Heat loss by both natural convection and radiation heat can be expressed as

$$\dot{Q} = hA_s(T_s - T_{\infty}) + \varepsilon A_s \sigma (T_s^4 - T_{surr}^4)$$
8 W = (6.696 W/m<sup>2</sup>.°C)(0.03 m<sup>2</sup>)(T\_s - 20)°C + (0.8)(0.03 m<sup>2</sup>)(5.67 × 10<sup>-8</sup>)[(T\_s + 273)<sup>4</sup> - (20 + 273 K)<sup>4</sup>]  
s solution is

Its solution is

*T*<sub>c</sub> = **42.6**°C

which is sufficiently close to the assumed value of  $45^{\circ}$ C in the evaluation of the properties and h.

(c) Horizontal, hot surface facing down This time we expect the surface temperature to be higher, and assume the surface temperature to be 50°C. We will check this assumption after obtaining result and repeat calculations with a better assumption, if necessary. The properties of air at the film temperature of (50+20)/2=35°C are (Table A-22)

$$k = 0.02625 \text{ W/m.°C}$$
  

$$\nu = 1.655 \times 10^{-5} \text{ m}^2/\text{s}$$
  

$$Pr = 0.7268$$
  

$$\beta = \frac{1}{T_f} = \frac{1}{(35 + 273)\text{K}} = 0.003247 \text{ K}^{-1}$$

The characteristic length in this case is, from part (b),  $L_c = 0.0429$  m. Then,

$$Ra = \frac{g\beta(T_s - T_{\infty})L_c^3}{v^2} \operatorname{Pr} = \frac{(9.81 \text{ m/s}^2)(0.003247 \text{ K}^{-1})(50 - 20 \text{ K})(0.0429 \text{ m})^3}{(1.655 \times 10^{-5} \text{ m}^2/\text{s})^2} (0.7268) = 200,200$$
$$Nu = 0.27Ra^{1/4} = 0.27(200,200)^{1/4} = 5.711$$
$$h = \frac{k}{L_c} Nu = \frac{0.02625 \text{ W/m.}^{\circ}\text{C}}{0.0429 \text{ m}} (5.711) = 3.494 \text{ W/m}^2.^{\circ}\text{C}$$

Considering both natural convection and radiation heat loses

$$\dot{Q} = hA_s(T_s - T_{\infty}) + \varepsilon A_s \sigma (T_s^4 - T_{surr}^4)$$
8 W = (3.494 W/m<sup>2</sup>.°C)(0.03 m<sup>2</sup>)(T\_s - 20)°C + (0.8)(0.03 m<sup>2</sup>)(5.67 × 10<sup>-8</sup>)[(T\_s + 273)<sup>4</sup> - (20 + 273 K)<sup>4</sup>]

Its solution is

 $T_{s} = 50.3^{\circ}C$ 

which is very close to the assumed value. Therefore, there is no need to repeat calculations.