Assumptions **1** This is a steady-flow process since there is no change with time. **2** Kinetic and potential energy changes are negligible. **3** The turbine is adiabatic and thus heat transfer is negligible.

Properties From the steam tables (Table A-6)

$$P_{1} = 12.5 \text{ MPa} T_{1} = 550^{\circ}\text{C}$$

$$h_{1} = 3476.5 \text{ kJ/kg} h_{2} = 1 \text{ MPa} T_{2} = 200^{\circ}\text{C}$$

$$h_{2} = 2828.3 \text{ kJ/kg} P_{3} = 100 \text{ kPa} T_{3} = 100^{\circ}\text{C}$$

$$h_{3} = 2675.8 \text{ kJ/kg}$$



Analysis The mass flow rate through the second stage is

$$\dot{m}_3 = \dot{m}_1 - \dot{m}_2 = 20 - 1 = 19 \text{ kg/s}$$

We take the entire turbine, including the connection part between the two stages, as the system, which is a control volume since mass crosses the boundary. Noting that one fluid stream enters the turbine and two fluid streams leave, the energy balance for this steady-flow system can be expressed in the rate form as

 $\underline{\dot{E}_{in}} - \underline{\dot{E}_{out}}_{Bate of net energy transfer} = \underbrace{\Delta \dot{E}_{system}}_{Rate of change in internal, kinetic, potential, etc. energies} = 0$ $\dot{E}_{in} = \dot{E}_{out}$ $\dot{m}_1 h_1 = \dot{m}_2 h_2 + \dot{m}_3 h_3 + \dot{W}_{out}$ $\dot{W}_{out} = \dot{m}_1 h_1 - \dot{m}_2 h_2 - \dot{m}_3 h_3$

Substituting, the power output of the turbine is

$$\dot{W}_{out} = (20 \text{ kg/s})(3476.5 \text{ kJ/kg}) - (1 \text{ kg/s})(2828.3 \text{ kJ/kg}) - (19 \text{ kg/s})(2675.8 \text{ kJ/kg})$$

= **15,860 kW**