8-60 Steam is expanded in an isentropic turbine. The work produced is to be determined.

Assumptions 1 This is a steady-flow process since there is no change with time. 2 The process is isentropic (i.e., reversible-adiabatic).

Analysis There is one inlet and two exits. We take the turbine as the system, which is a control volume since mass crosses the boundary. The energy balance for this steady-flow system can be expressed in the rate form as

$$\underbrace{\dot{E}_{\text{in}} - \dot{E}_{\text{out}}}_{\text{Rate of net energy transfer}} = \underbrace{\Delta \dot{E}_{\text{system}}^{\pi_0 \text{ (steady)}}}_{\text{Rate of change in internal, kinetic, potential, etc. energies}} = 0$$

$$\frac{\dot{E}_{\text{in}} = \dot{E}_{\text{out}}}{\dot{m}_1 h_1 = \dot{m}_2 h_2 + \dot{m}_3 h_3 + \dot{W}_{\text{out}}}$$

$$\frac{\dot{W}_{\text{out}} = \dot{m}_1 h_1 - \dot{m}_2 h_2 - \dot{m}_3 h_3}{\dot{W}_{\text{out}}}$$

From a mass balance,

by

$$\dot{m}_2 = 0.05\dot{m}_1 = (0.05)(5 \text{ kg/s}) = 0.25 \text{ kg/s}$$

 $\dot{m}_3 = 0.95\dot{m}_1 = (0.95)(5 \text{ kg/s}) = 4.75 \text{ kg/s}$

Noting that the expansion process is isentropic, the enthalpies at three states are determined as follows:

$$P_{3} = 50 \text{ kPa} \begin{cases} h_{3} = 2682.4 \text{ kJ/kg} \\ s_{3} = 100^{\circ}\text{C} \end{cases} \begin{array}{c} h_{3} = 2682.4 \text{ kJ/kg} \\ s_{3} = 7.6953 \text{ kJ/kg} \cdot \text{K} \end{cases} \text{ (Table A - 6)} \\ P_{1} = 4 \text{ MPa} \\ s_{1} = s_{3} = 7.6953 \text{ kJ/kg} \cdot \text{K} \end{cases} h_{1} = 3979.3 \text{ kJ/kg} \text{ (Table A - 6)} \\ P_{2} = 700 \text{ kPa} \\ s_{2} = s_{3} = 7.6953 \text{ kJ/kg} \cdot \text{K} \end{cases} h_{2} = 3309.1 \text{ kJ/kg} \text{ (Table A - 6)} \\ \end{array}$$

Substituting,

$$\dot{W}_{out} = \dot{m}_1 h_1 - \dot{m}_2 h_2 - \dot{m}_3 h_3$$

= (5 kg/s)(3979.3 kJ/kg) - (0.25 kg/s)(3309.1 kJ/kg) - (4.75 kg/s)(2682.4 kJ/kg)
= **6328 kW**



