**7-39** Water vapor is expanded in a turbine during which the entropy remains constant. The enthalpy difference is to be determined.

Analysis The initial state is superheated vapor and thus

$$P_{1} = 6 \text{ MPa} \ \ h_{1} = 3178.3 \text{ kJ/kg} T_{1} = 400^{\circ}\text{C} \ \ s_{1} = 6.5432 \text{ kJ/kg} \cdot \text{K}$$
(Table A - 6)

The entropy is constant during the process. The final state is a mixture since the entropy is between  $s_f$  and  $s_g$  for 100 kPa. The properties at this state are (Table A-5)

$$\begin{aligned} x_2 &= \frac{s_2 - s_f}{s_{fg}} = \frac{(6.5432 - 1.3028) \text{ kJ/kg} \cdot \text{K}}{6.0562 \text{ kJ/kg} \cdot \text{K}} = 0.8653 \\ h_2 &= h_f + x_2 h_{fg} = 417.51 + (0.8653)(2257.5) = 2370.9 \text{ kJ/kg} \end{aligned}$$

The change in the enthalpy across the turbine is then

$$\Delta h = h_2 - h_1 = 2370.9 - 3178.3 = -807.4 \text{ kJ/kg}$$



**7-40** R-134a undergoes a process during which the entropy is kept constant. The final temperature and internal energy are to be determined.

Analysis The initial entropy is

$$\left. \begin{array}{l} T_1 = 25^{\circ}\text{C} \\ P_1 = 600 \text{ kPa} \end{array} \right\} \quad s_1 = 0.9341 \text{ kJ/kg} \cdot \text{K} \quad \text{(Table A - 13)}$$

The entropy is constant during the process. The final state is a mixture since the entropy is between  $s_f$  and  $s_g$  for 100 kPa. The properties at this state are (Table A-12)

$$T_{2} = T_{\text{sat} @ 100 \text{ kPa}} = -26.37 \,^{\circ}\text{C}$$

$$x_{2} = \frac{s_{2} - s_{f}}{s_{fg}} = \frac{(0.9341 - 0.07188) \text{ kJ/kg} \cdot \text{K}}{0.87995 \text{ kJ/kg} \cdot \text{K}} = 0.9799$$

$$u_{2} = u_{f} + x_{2}u_{fg} = 17.21 + (0.9799)(197.98) = 211.2 \text{ kJ/kg}$$

