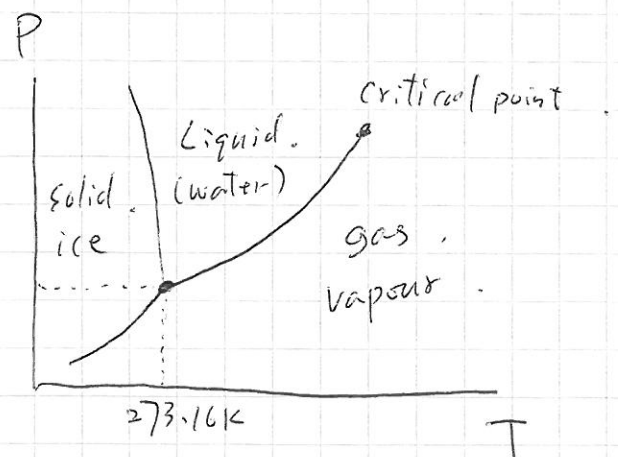
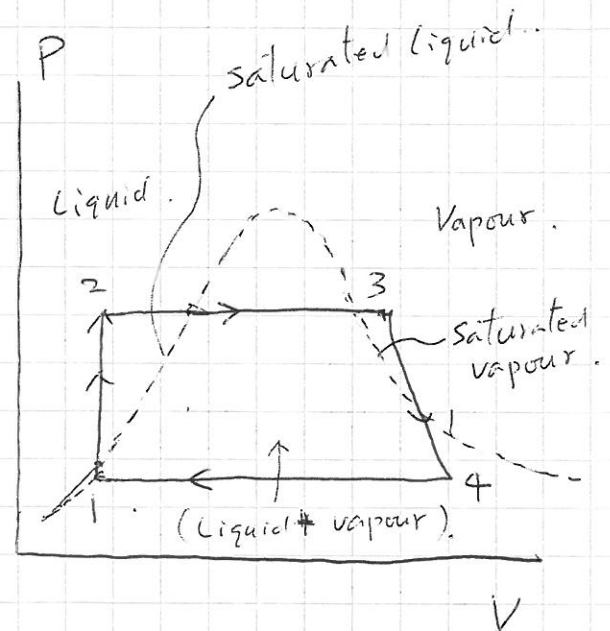
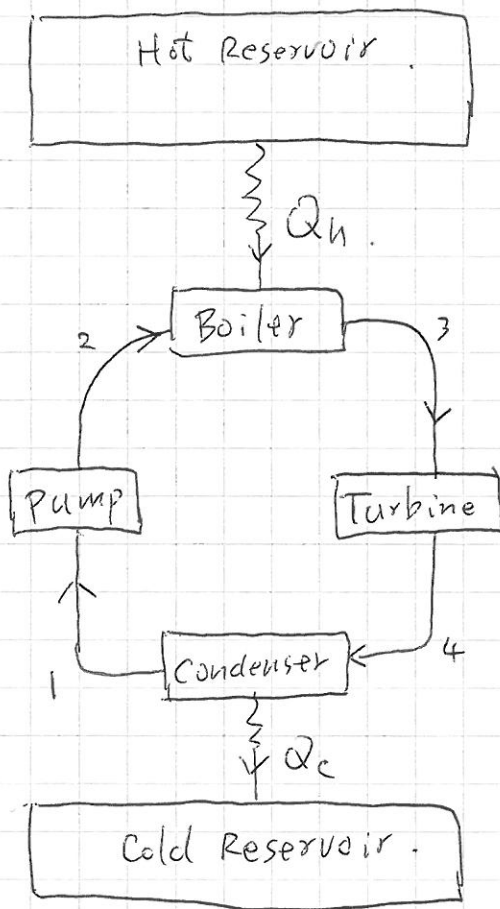


Phys 344

Lecture 19. The Steam Engine.

- Rankine cycle of water (NOT ideal gas!)



1 $\rightarrow$ 2. ~~isobaric (constant P)~~

also nearly adiabatic (and quasistatic). (const. S)

3 $\rightarrow$ 4. Adiabatic.

$$\therefore e = \frac{Q_h - Q_c}{Q_h} = 1 - \frac{Q_c}{Q_h} = 1 - \frac{H_4 - H_1}{H_3 - H_2} \approx 1 - \frac{H_4 - H_1}{H_3 - H_1}$$

Note: ΔH = Heat absorbed when $P = \text{constant}$.

$$H = U + PV$$

$$\Delta H = \Delta U + P\Delta V = \Delta U - \underbrace{W}_{\substack{\uparrow \\ \text{work on system}}} = Q$$

How do we calculate e ?

— use the steam tables. to find $H_1, (H_2), H_3, H_4$

$$H_1 = H_2, \quad S_3 = S_4.$$

• saturated water/vapour — 2 phases coexist. (same S .)

temperature
can be determined
by pressure.

and vice versa.

$$H = H(T), \quad S = S(T).$$

• superheated steam — H_2O gas.

Mixture of water and vapour.

Volume varies depending on $\left(\frac{m_w}{m_v}\right)$.

$T \sim P$ relation is well defined.

$P = f(T)$ — unique.

We need to specify P , and T .

$$H = H(P, T), \quad S = S(P, T).$$

(Note: For a given amount of H_2O , ~~1 kg~~.)

Note: The table is good for $\Delta H, \Delta S$

but not necessarily for S, H .

e.g: $\left\{ \begin{array}{l} P_1 = 0.023 \text{ bar} \\ T_1 = 20^\circ\text{C} \end{array} \right\} \left\{ \begin{array}{l} \text{(The partial pressure of } H_2O \text{)} \\ \text{in the atmosphere} \end{array} \right\}$
 all water (very little vapour)

$$P_2 = P_3 = 300 \text{ bars}$$

(1) — water

$$T_{\max} = T_3 = 600^\circ\text{C}$$

(2) — water

(3) — steam

Consider 1 kg of H_2O .

(4) — mixture

$$H_1 = 84 \text{ kJ}$$

$$H_3 = 3444 \text{ kJ}$$

$$S_3 = 6.233 \text{ kJ/K}$$

$$4: \left\{ \begin{array}{l} 0.023 \text{ bar} \\ @ 20^\circ\text{C} \end{array} \right.$$

$$S_4 = S_3 \Rightarrow$$

$$x S_{\text{water}} + (1-x) S_{\text{steam}} = S_4$$

$$0.297x + 8.667(1-x) = 6.233$$

Solve for x:

$$0.297x + 8.667 - 8.667x = 6.233$$

$$x = \frac{8.667 - 6.233}{8.667 - 0.297} = 0.29$$

(2) 4:

water: 29%, Vapour: 71%

$$H_4 = 0.29 H_{\text{water}} + 0.71 H_{\text{vapour}}$$

$$= 0.29 \times 84 + 0.71 \times 2538 = 1826 \text{ kJ}$$

19-4.

$$\therefore e = 1 - \frac{1826 - 84}{3444 - 84} = 48\%$$

Note: For liquid water, H is not sensitive to P .

$$(\because H = U + PV, \quad V \text{ is small})$$

Next: Real Refrigerator.

— Reverse of Rankine cycle.

— can't use water/steam

e.g. CFC.

HFC-134a.

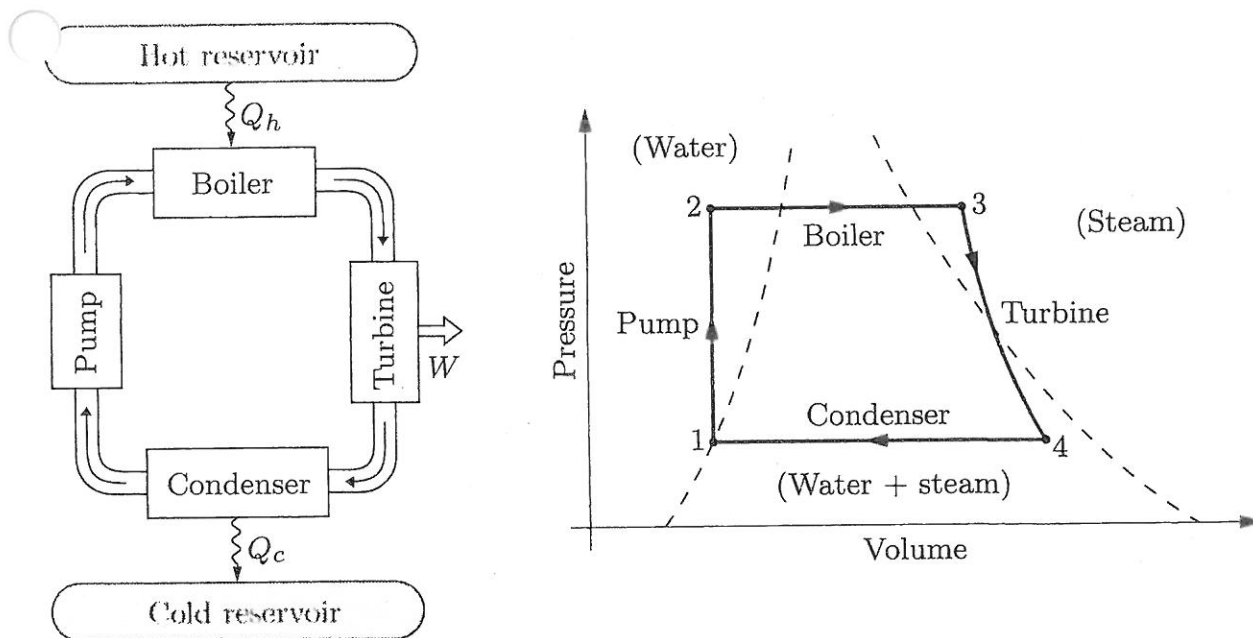


Figure 4.8. Schematic diagram of a steam engine and the associated PV cycle (not to scale), called the **Rankine cycle**. The dashed lines show where the fluid is liquid water, where it is steam, and where it is part water and part steam.

T (°C)	P (bar)	H_{water} (kJ)	H_{steam} (kJ)	S_{water} (kJ/K)	S_{steam} (kJ/K)
0	0.006	0	2501	0	9.156
10	0.012	42	2520	0.151	8.901
20	0.023	84	2538	0.297	8.667
30	0.042	126	2556	0.437	8.453
50	0.123	209	2592	0.704	8.076
100	1.013	419	2676	1.307	7.355

Table 4.1. Properties of saturated water/steam. Pressures are given in bars, where 1 bar = 10^5 Pa $\approx$ 1 atm. All values are for 1 kg of fluid, and are measured relative to liquid water at the triple point (0.01°C and 0.006 bar). Excerpted from Keenan et al. (1978).

P (bar)		Temperature (°C)				
		200	300	400	500	600
1.0	H (kJ)	2875	3074	3278	3488	3705
	S (kJ/K)	7.834	8.216	8.544	8.834	9.098
3.0	H (kJ)	2866	3069	3275	3486	3703
	S (kJ/K)	7.312	7.702	8.033	8.325	8.589
10	H (kJ)	2828	3051	3264	3479	3698
	S (kJ/K)	6.694	7.123	7.465	7.762	8.029
30	H (kJ)		2994	3231	3457	3682
	S (kJ/K)		6.539	6.921	7.234	7.509
100	H (kJ)			3097	3374	3625
	S (kJ/K)			6.212	6.597	6.903
300	H (kJ)			2151	3081	3444 H_3
	S (kJ/K)			4.473	5.791	6.233 S_3

Table 4.2. Properties of superheated steam. All values are for 1 kg of fluid, and are measured relative to liquid water at the triple point. Excerpted from Keenan et al. (1978).

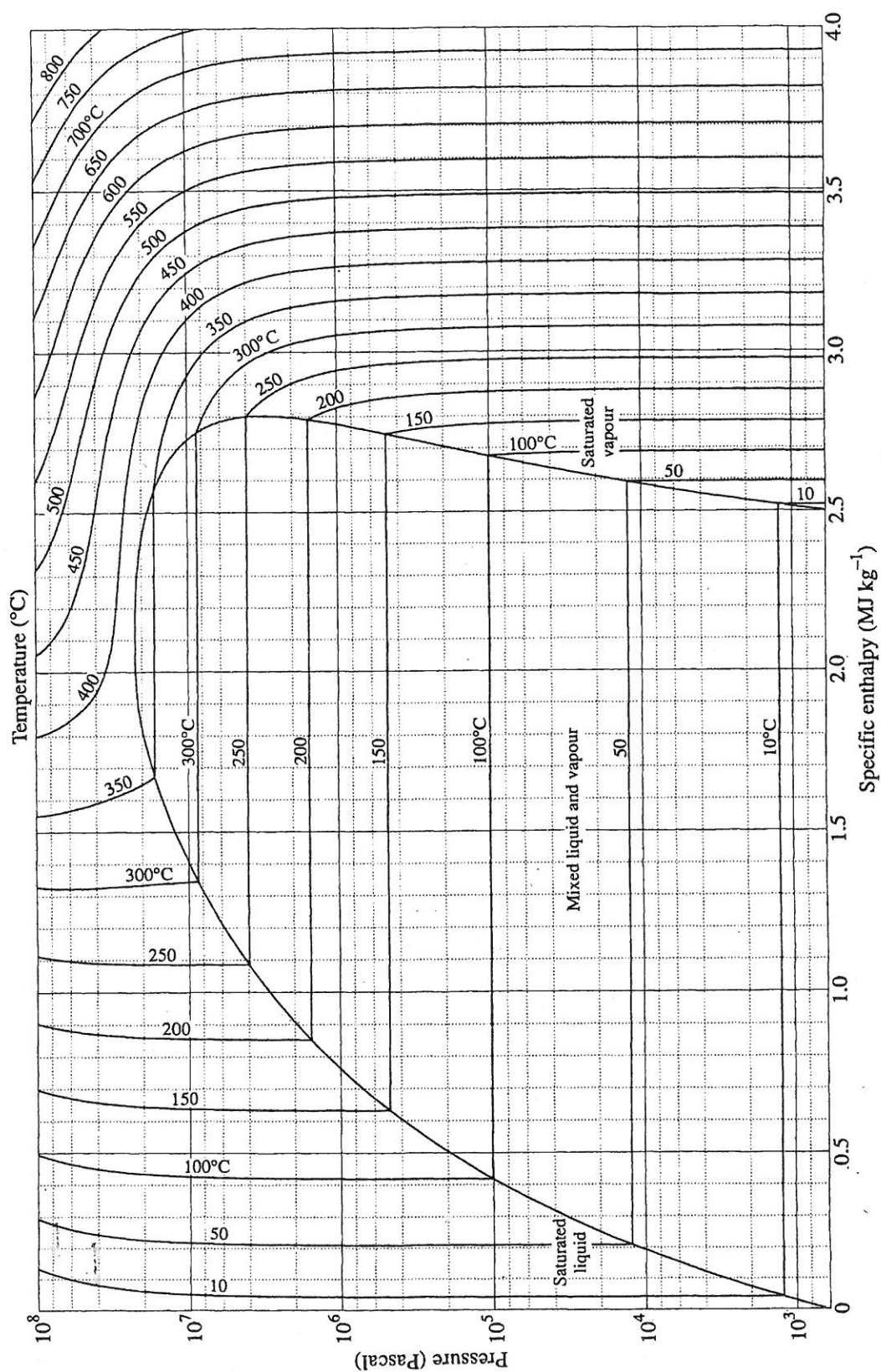


Fig. B.6