

Spontaneous Change

For a system in thermal equilibrium with its surroundings,

$$dS \geq \frac{\delta q}{T} \quad \text{Clausius inequality}$$

At constant volume:

$$dq_V = dU \quad \text{no work}$$

$$TdS - dU \geq 0$$

$$(dS)_{U,V} \geq 0 \quad \text{isolated system}$$

$$(dU)_{S,V} \leq 0$$

At constant pressure:

$$dq_P = dH \quad \text{PV work only}$$

$$TdS - dH \geq 0$$

$$(dH)_{S,P} \leq 0$$

For convenience, define:

$$A = U - TS$$

$$dA = dU - TdS - SdT$$

$$G = H - TS$$

$$dG = dH - TdS - SdT$$

Then the conditions for spontaneous change become:

$$(dA)_{T,V} \leq 0$$

$$(dG)_{T,P} \leq 0$$

Helmholtz Energy A

Helmholtz energy; Helmholtz free energy; Helmholtz function;
Maximum work function A for Arbeit

For spontaneous change at constant T and V

$$dA = dU - TdS \leq 0$$

Note that it is the *total* function A that tends to a minimum;
this is *not* the same as minimizing U and maximizing S .

Maximum Work

Combine $dU = \delta q + \delta w$ and $TdS \geq \delta q$

$$\Rightarrow dU \leq TdS + \delta w$$

equality for
reversible change

Word done by
the system

$$(-\delta w) \leq TdS - dU$$

$$(-\delta w)_{\max} = TdS - \delta q_{\text{rev}} - \delta w_{\text{rev}} = -\delta w_{\text{rev}}$$

A system does maximum work when it is operating reversibly.

But $(dA)_T = dU - TdS = dU - \delta q_{\text{rev}} = \delta w_{\text{rev}}$

Therefore, for macroscopic changes

$$-w_{\max} = -\Delta A = T\Delta S - \Delta U \quad \text{constant } T$$

$(-w)$ can be more or less than ΔU according to the sign of ΔS .

For $\Delta S > 0$, heat flows into the system to fuel the extra work.

Gibbs Energy G

Gibbs free energy, Gibbs function

- ❖ Very important in chemistry since it tells whether a particular reaction can proceed at a given T and P .

For spontaneous change,

$$(dG)_{T,P} \leq 0 \quad \Delta G = G_{\text{products}} - G_{\text{reactants}} \leq 0$$

$\Delta G_{T,P}$ for reactions can be calculated from tabulated data

$$\Delta G^\circ(T) = \Delta H^\circ(T) - T\Delta S^\circ(T)$$

| If ΔH is | and ΔS is | then ΔG | the reaction proceeds |
|------------------|-------------------|-----------------|------------------------------|
| -ve | +ve | < 0 | at all temperatures |
| +ve | -ve | > 0 | at no temperatures |
| -ve | -ve | ... | if $T < \Delta H / \Delta S$ |
| +ve | +ve | ... | if $T > \Delta H / \Delta S$ |

Maximum Work:

$$(dG)_T = dH - TdS$$

$$(dG)_{T,P} = dU + PdV - TdS$$

$$= \delta q_{\text{rev}} + \delta w_{\text{rev}} + PdV - TdS$$

$$= \delta w_{\text{rev}} + PdV$$

$$= \delta w_{\text{max}} (\text{non-PV})$$

$$\Delta w_{\text{max}} (\text{non-PV}) = \Delta G \quad \text{constant } T, P$$

Basic Thermodynamic Relations 1

Laws $dU = \delta q - PdV$... (1)

$$dS = \delta q_{\text{rev}} / T \quad \dots (2)$$

Definitions $H = U + PV$... (3)

$$A = U - TS \quad \dots (4)$$

$$G = H - TS \quad \dots (5)$$

Fundamental Equations

$$dU = TdS - PdV \quad \dots (6)$$

$$dH = TdS + VdP \quad \dots (7)$$

$$dA = -SdT - PdV \quad \dots (8)$$

$$dG = -SdT + VdP \quad \dots (9)$$

Partial Differentials

$$\left(\frac{\partial U}{\partial S} \right)_V = T \quad \left(\frac{\partial U}{\partial V} \right)_S = -P$$

$$\left(\frac{\partial H}{\partial S} \right)_P = T \quad \left(\frac{\partial H}{\partial P} \right)_S = V$$

$$\left(\frac{\partial A}{\partial T} \right)_V = -S \quad \left(\frac{\partial A}{\partial V} \right)_T = -P$$

$$\left(\frac{\partial G}{\partial T} \right)_P = -S \quad \left(\frac{\partial G}{\partial P} \right)_T = V$$

Basic Thermodynamic Relations 2

Maxwell Relations

From (6) $\left(\frac{\partial T}{\partial V}\right)_S = -\left(\frac{\partial P}{\partial S}\right)_V \dots(10)$

From (7) $\left(\frac{\partial T}{\partial P}\right)_S = \left(\frac{\partial V}{\partial S}\right)_P \dots(11)$

From (8) $\left(\frac{\partial S}{\partial V}\right)_T = \left(\frac{\partial P}{\partial T}\right)_V \dots(12)$

From (9) $-\left(\frac{\partial S}{\partial P}\right)_T = \left(\frac{\partial V}{\partial T}\right)_P \dots(13)$

Thermodynamic Equation of State

$$dU = TdS - PdV \dots(6)$$

$$\left(\frac{\partial U}{\partial V}\right)_T = T\left(\frac{\partial S}{\partial V}\right)_T - P$$

Substituting (12) $\left(\frac{\partial U}{\partial V}\right)_T = T\left(\frac{\partial P}{\partial T}\right)_V - P$

$$\left(\frac{\partial U}{\partial V}\right)_T = T\left(\frac{\alpha}{\kappa}\right) - P$$

How Free Energy Depends on T

$$G = H - TS \quad \dots(1) \quad \text{definition}$$

$$\Delta G = \Delta H - T\Delta S \quad \dots(2) \quad \text{constant } T$$

$$dG = VdP - SdT \quad \dots(3) \quad \text{fundamental eqn.}$$

$$\left(\frac{\partial G}{\partial T}\right)_P = -S = \frac{G - H}{T} \quad \text{from (1)}$$

$$\therefore \left(\frac{\partial G}{\partial T}\right)_P - \frac{G}{T} = -\frac{H}{T} \quad \dots(4)$$

$$\text{But} \quad \left(\frac{\partial(G/T)}{\partial T}\right)_P = \frac{1}{T}\left(\frac{\partial G}{\partial T}\right)_P - \frac{G}{T^2} \quad \dots(5)$$

Gibbs-Helmholtz
Equation

$$\left(\frac{\partial(G/T)}{\partial T}\right)_P = -\frac{H}{T^2}$$

substitute
(4) in (5)

alternative form:

$$\left(\frac{\partial(G/T)}{\partial(1/T)}\right)_P = H$$

By applying the Gibbs-Helmholtz equation to both reactants and products of a chemical reaction,

$$\Rightarrow \left(\frac{\partial(\Delta G/T)}{\partial T}\right)_P = -\frac{\Delta H}{T^2}$$

How Free Energy Depends on P

$$\left(\frac{\partial G}{\partial P}\right)_T = V$$

$$\Delta G = G_2 - G_1 = \int_1^2 V dP$$

For solids and liquids V does not change much with P , so

$$G_2(T) \approx G_1(T) + V(P_2 - P_1)$$

For a perfect gas $V = \frac{nRT}{P}$

$$\Delta G_T = nRT \ln(P_2 / P_1)$$

$$G = G^\circ(T) + nRT \ln(P / P^\circ)$$

where G° is the **standard free energy** defined at $P^\circ=1$ bar

The chemical potential for a pure substance is the molar Gibbs energy:

$$\mu = \bar{G} = \frac{G}{n}$$

\therefore For a perfect gas

$$\mu = \mu^\circ + RT \ln(P / P^\circ)$$

The Chemical Potential

So far, our thermodynamic relations apply to **closed** systems. However, G , U , H , etc. are **extensive** properties.

Partial molar quantities are used to describe quantities which depend on composition.

$$\bar{J}_i = \left(\frac{\partial J}{\partial n_i} \right)_{T,P,n_{j \neq i}} \quad J = U, H, S, A, G, V$$

$$J = \sum_i n_i \bar{J}_i$$

In general

$$dG = \left(\frac{\partial G}{\partial P} \right)_{T,n_1,n_2,\dots} dP + \left(\frac{\partial G}{\partial T} \right)_{P,n_1,n_2,\dots} dT + \left(\frac{\partial G}{\partial n_1} \right)_{T,P,n_2,\dots} dn_1 + \left(\frac{\partial G}{\partial n_2} \right)_{T,P,n_1,n_3,\dots} dn_2 + \dots$$

Chemical Potential

$$\mu_i = \left(\frac{\partial G}{\partial n_i} \right)_{P,T,n_{j \neq i}}$$

Fundamental Equations

$$dU = TdS - PdV + \sum \mu_i dn_i$$
$$dH = TdS + VdP + \sum \mu_i dn_i$$

etc.

$$\Rightarrow \mu_i = \left(\frac{\partial U}{\partial n_i} \right)_{V,S} = \left(\frac{\partial H}{\partial n_i} \right)_{P,S} = \left(\frac{\partial A}{\partial n_i} \right)_{V,T}$$

Free Energy of Mixing 1

Consider the mixing of two *ideal* gases A and B at constant T and P .

Before: $G_1 = n_A \mu_A (\text{pure}) + n_B \mu_B (\text{pure})$

where $\mu_A (\text{pure}) = \mu_A^\circ + RT \ln(P / P_0)$

After mixing: $G_A = n_A \left\{ \mu_A^\circ + RT \ln(p_A / P_0) \right\}$
 $= n_A \left\{ \mu_A^\circ + RT \ln(P / P_0) + RT \ln \chi_A \right\}$

$= n_A \mu_A (\text{pure}) + n_A RT \ln \chi_A$

$G_2 = G_A + G_B < G_1$

negative

Change:

$\Delta G_{\text{mix}} = G_2 - G_1$

$= n_A RT \ln \chi_A + n_B RT \ln \chi_B$

$= nRT (\chi_A \ln \chi_A + \chi_B \ln \chi_B)$

$\Delta G_{\text{mix}} = nRT (\chi_A \ln \chi_A + \chi_B \ln \chi_B)$

$\Delta G_{\text{mix}} < 0$ Mixing is spontaneous.

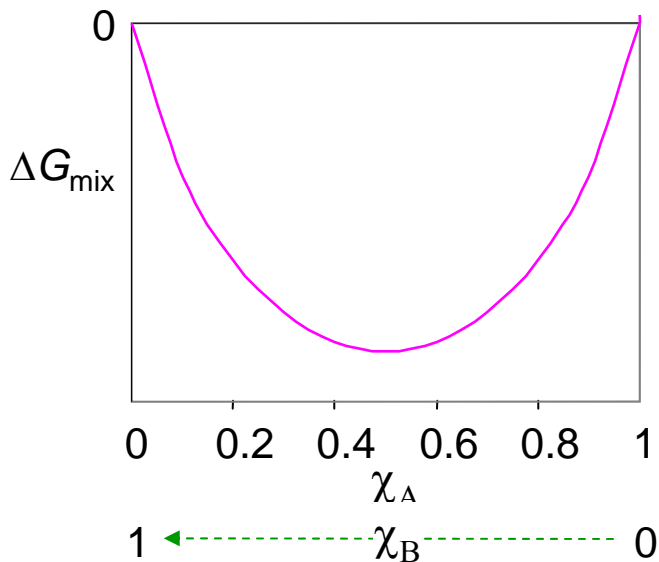
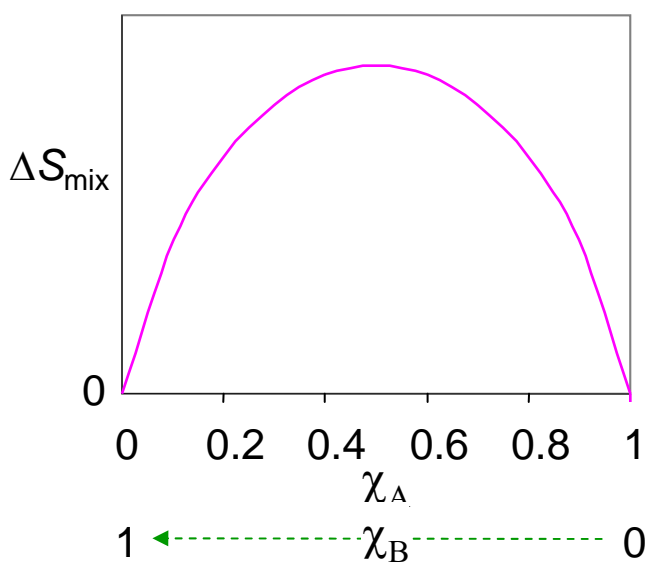
Entropy of Mixing $\Delta S_{\text{mix}} = -(\partial \Delta G_{\text{mix}} / \partial T)_{P, n_i} = -nR \sum \chi_i \ln \chi_i$

Enthalpy of Mixing $\Delta H_{\text{mix}} = \Delta G_{\text{mix}} + T \Delta S_{\text{mix}} = 0$

Similarly, $\Delta U_{\text{mix}} = \Delta V_{\text{mix}} = 0$ for ideal gases and solutions

Free Energy of Mixing 2

For a binary system, ΔG_{mix} is at its **minimum** and ΔS_{mix} at its **maximum** when $\chi_A = \chi_B = 0.5$

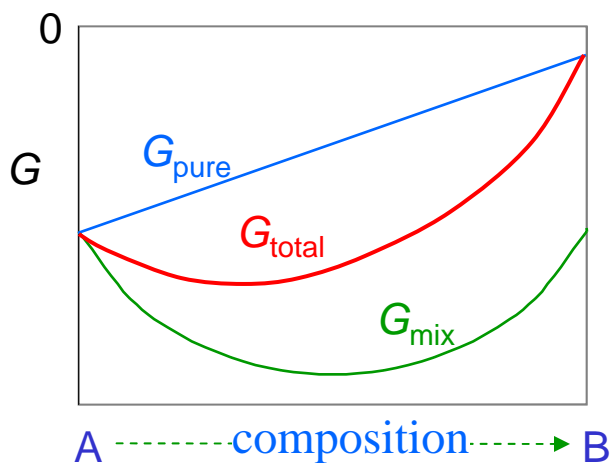


Equilibrium and Mixing:

Consider an equilibrium between two ideal gases $A \rightleftharpoons B$

$$G = G_A(\text{pure}) + G_B(\text{pure}) + \Delta G_{\text{mix}}$$

$$= n(\chi_A \mu_A + \chi_B \mu_B) + nRT(\chi_A \ln \chi_A + \chi_B \ln \chi_B)$$



The equilibrium composition is determined by the minimum in G_{total} .

Reaction Equilibrium 1

Consider $A \rightleftharpoons B$

Suppose an amount dx of A turns into B.

Then $(dG)_{T,P} = \mu_A dn_A + \mu_B dn_B = -\mu_A dx + \mu_B dx$

$$\Rightarrow \left(\frac{\partial G}{\partial x} \right)_{T,P} = \mu_B - \mu_A$$

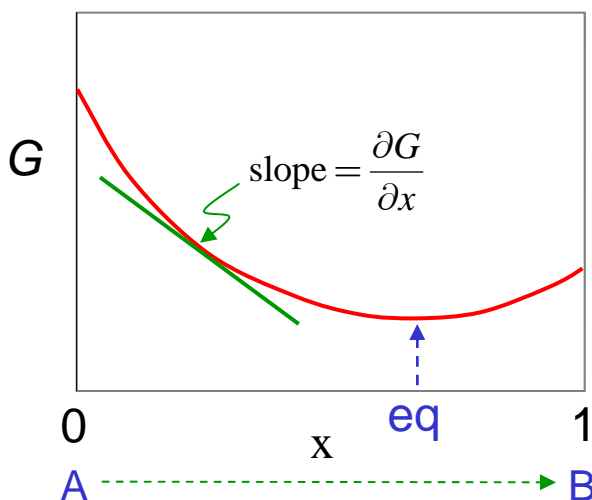
μ_A and μ_B depend on composition, and therefore change during the reaction.

If $\mu_A > \mu_B$ the reaction proceeds from $A \rightarrow B$.

If $\mu_A < \mu_B$ the reaction proceeds from $B \rightarrow A$.

At equilibrium

$$\mu_A = \mu_B$$



$$\mu_A^\circ + RT \ln(p_A^{\text{eq}} / P^\circ) = \mu_B^\circ + RT \ln(p_B^{\text{eq}} / P^\circ)$$

$$RT \ln(p_A^{\text{eq}} / p_B^{\text{eq}}) = \mu_B^\circ - \mu_A^\circ = \Delta \bar{G}_{\text{rxn}}^\circ$$

$$\frac{p_B^{\text{eq}}}{p_A^{\text{eq}}} = \exp(-\Delta \bar{G}_{\text{rxn}}^\circ / RT)$$

Reaction Equilibrium 2

A reaction such as $2A + 3B \rightarrow C + 2D$ can be written as

$$0 = -2A - 3B + C + 2D$$

or completely generally as $0 = \sum_i \nu_i R_i = 0$

Then
$$\left(\frac{\partial G}{\partial \xi} \right)_{T,P} = \sum_i \nu_i \mu_i$$

and at equilibrium,
$$\sum_i \nu_i \mu_i = 0$$

$$\sum_i \left(\nu_i \mu_i^\circ + \nu_i RT \ln \frac{P_i^{\text{eq}}}{P^\circ} \right) = 0$$

$$\Delta \bar{G}_{\text{rxn}}^\circ + RT \ln \left[\prod_i \left(\frac{P_i}{P^\circ} \right)_{\text{eq}}^{\nu_i} \right] = 0$$

$$\Delta \bar{G}_{\text{rxn}}^\circ = -RT \ln K$$

$$K = \prod_i \left(\frac{P_i}{P^\circ} \right)_{\text{eq}}^{\nu_i}$$